

Granular flows down inclines: how different bases produce widely different scaling of mass flow rate with depth

Michel Louge



Second International Granular Flow Workshop, Guiyang, China

Tuesday, August 22, 2017

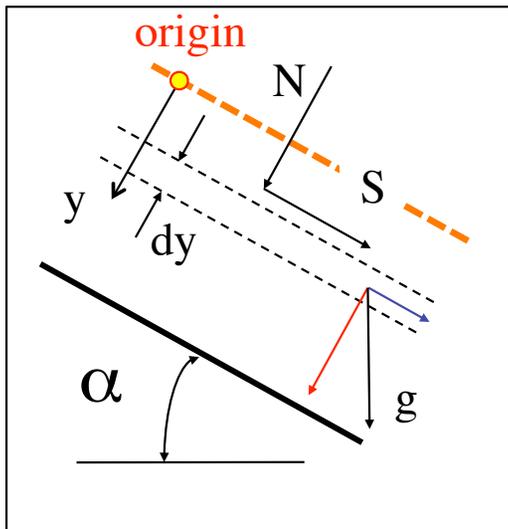
ML, A. Valance, P. Lancelot, R. Delannay, O. Artières, PRE 92, 022204 (2015)

Dense inclined granular flow



Steady, fully-developed force balance

Steady ($\partial / \partial t \equiv 0$), fully-developed ($\partial / \partial x \equiv 0$) flow



Force balance

$$\frac{dS}{dy} = \rho g \sin \alpha$$

$$\frac{dN}{dy} = \rho g \cos \alpha$$

$$S = \rho g y \sin \alpha$$

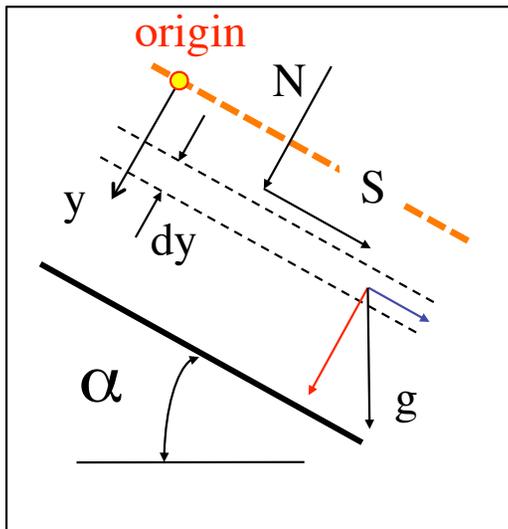
$$N = \rho g y \cos \alpha$$

$$\mu_{\text{eff}} = \frac{S}{N} = \tan \alpha$$



Newtonian viscous fluid

laminar flow



Force balance

$$\frac{dS}{dy} = \rho g \sin \alpha$$

$$\frac{dN}{dy} = \rho g \cos \alpha$$

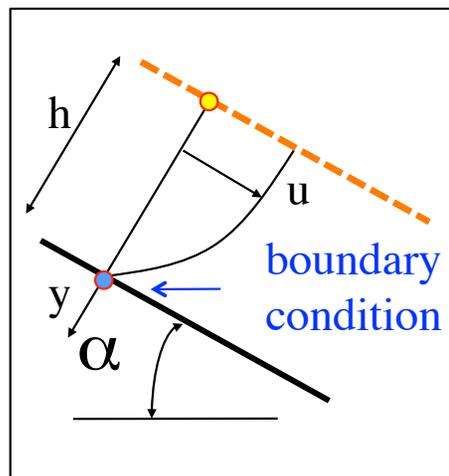
$$S = \rho g y \sin \alpha$$

$$N = \rho g y \cos \alpha$$

$$\mu_{\text{eff}} = \frac{S}{N} = \tan \alpha$$

Constitutive relation

$$S = -\mu \frac{du}{dy}$$

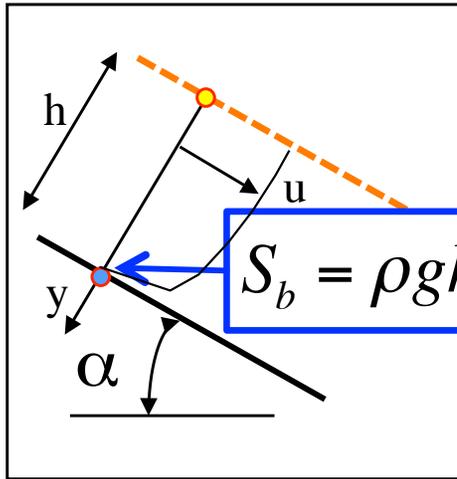


$$u = \frac{\rho g \sin \alpha}{2\mu} (h^2 - y^2)$$

$$\frac{\dot{m}}{W} = \left(\frac{\rho^2 g \sin \alpha}{3\mu} \right) h^3$$

Newtonian viscous fluid

turbulent flow



$$S_b = \rho g h \sin \alpha = \text{cst} \times \rho \bar{u}^2$$

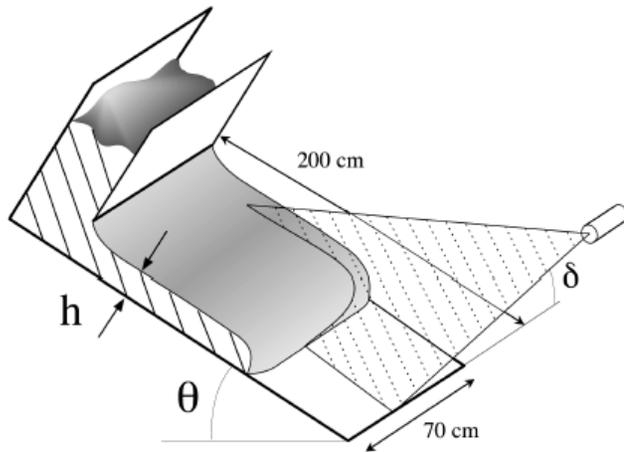
$$\text{cst} = \left(u^* / \bar{u} \right)^2 \approx 3 \cdot 10^{-3}$$

$$\frac{\dot{m}}{W} = \rho \bar{u} h = \rho \sqrt{\frac{g \sin \alpha}{\text{cst}}} h^{3/2}$$



Ludwig Prandtl

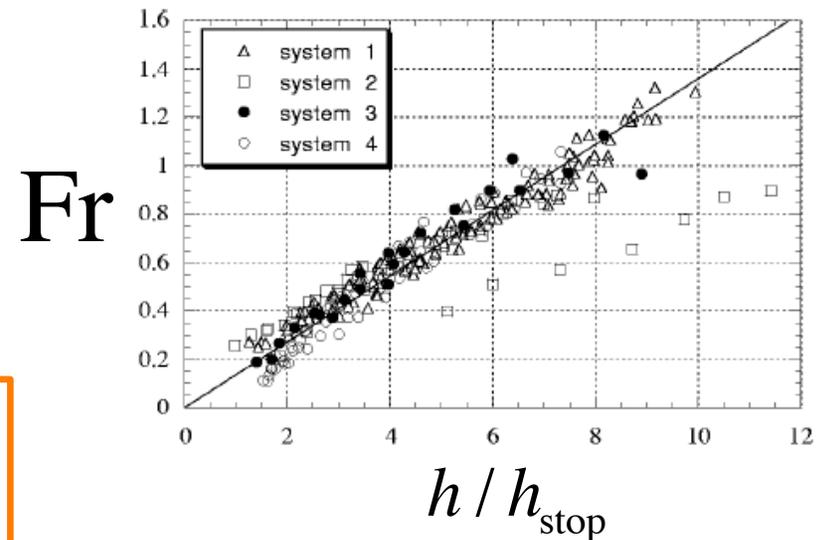
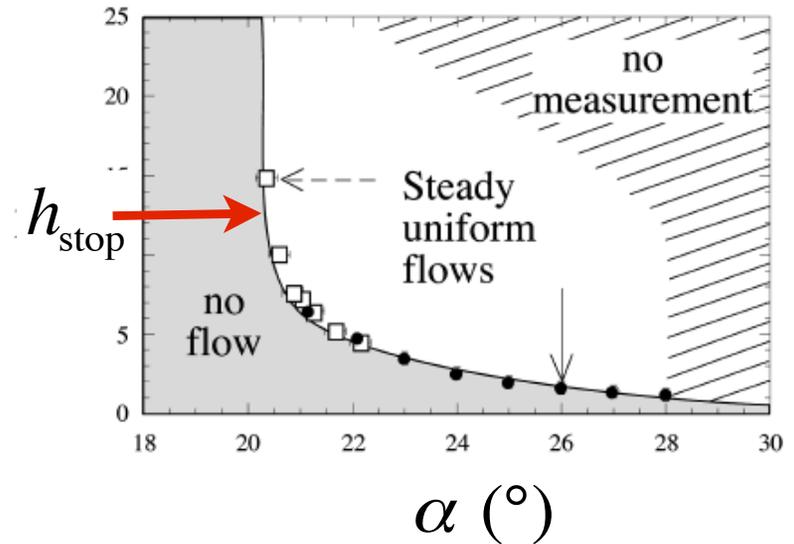
Shallow flows, far sidewalls, bumpy base



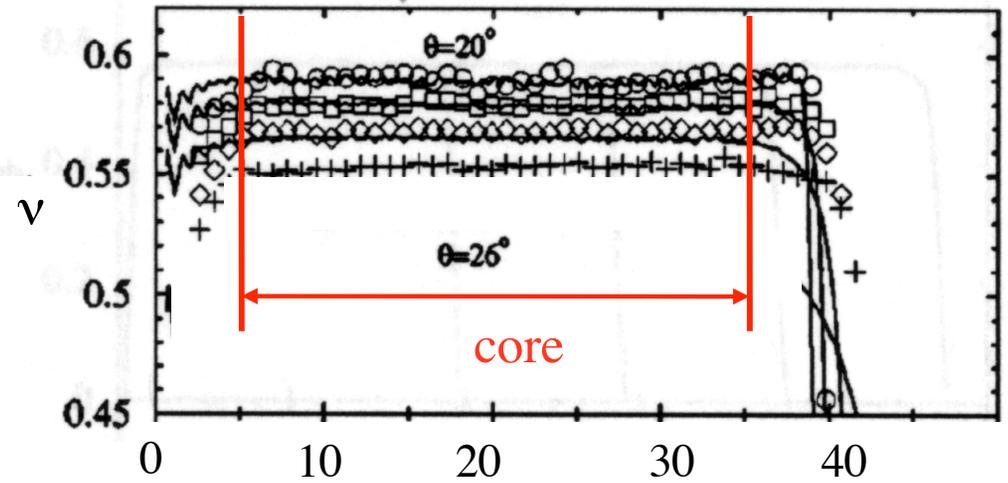
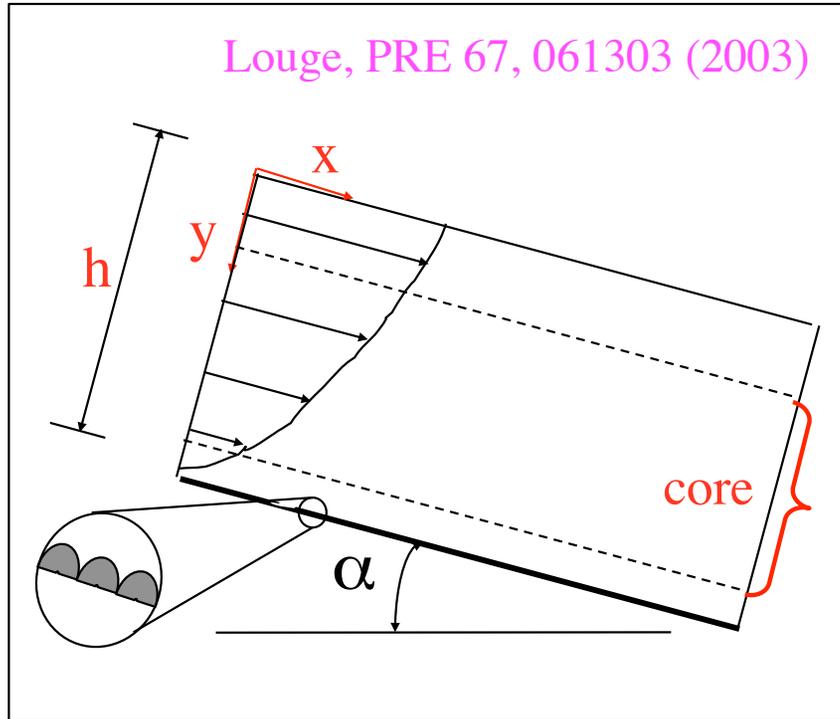
Pouliquen, Phys. Fluids 1999

$$\frac{\dot{m}}{W} \propto \text{cst } \rho_s \bar{v} \frac{\sqrt{g \cos \alpha}}{h_{\text{stop}}} h^{5/2}$$

$$\text{Fr} \equiv \frac{\bar{u}}{\sqrt{N / \rho}} = \frac{\bar{u}}{\sqrt{gh \cos \alpha}}$$



Shallow flows, far sidewalls, bumpy base



Silbert, et al. PRE 2001

$$\frac{\dot{m}}{W} \propto \text{cst } \rho_s \bar{v} \frac{\sqrt{g \cos \alpha}}{h_{\text{stop}}} h^{5/2}$$

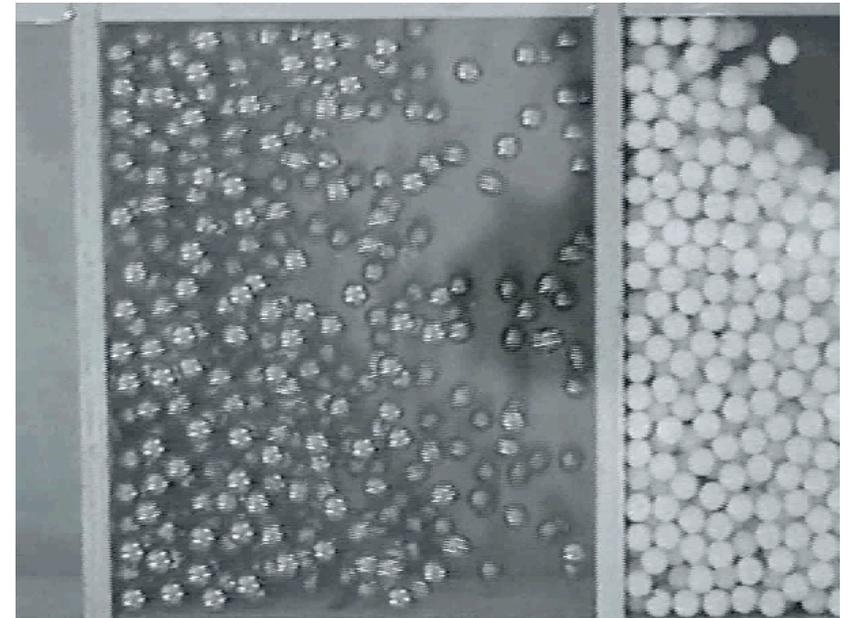
$$20^\circ < \alpha < 26^\circ$$

$$0.595 > v > 0.545$$



Leo Silbert

Granular temperature



“temperature” $T = \frac{1}{3} \overline{u'_i u'_i}$

fluctuation velocity u'_i

Transport coefficients



Stuart Savage



James Jenkins

viscosity

$$\mu = \rho_s d \sqrt{T} f_1(\nu; g_{12})$$

conductivity

$$\kappa = \rho_s d \sqrt{T} f_2(\nu; g_{12})$$

dissipation

$$\gamma = f_3(\nu; g_{12}; e) \rho_s T^{3/2} / d$$

equation of state

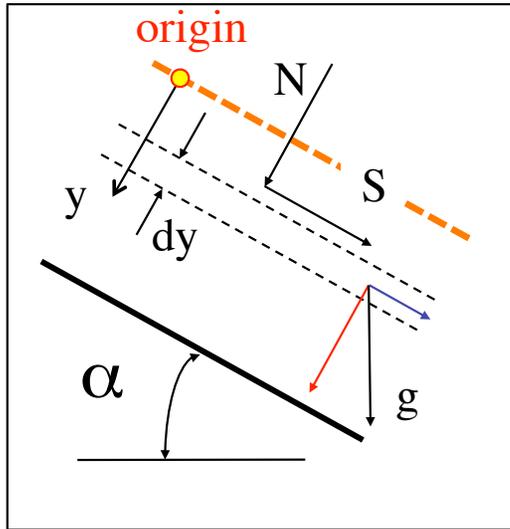
$$N = f_4(\nu; g_{12}) \rho_s T$$

Kinetic theory cartoon

Ralph Bagnold



viscosity



bumpy base

$$S = \rho_s v g y \sin \alpha = -f_1 \rho_s d \sqrt{T} \frac{du}{dy}$$

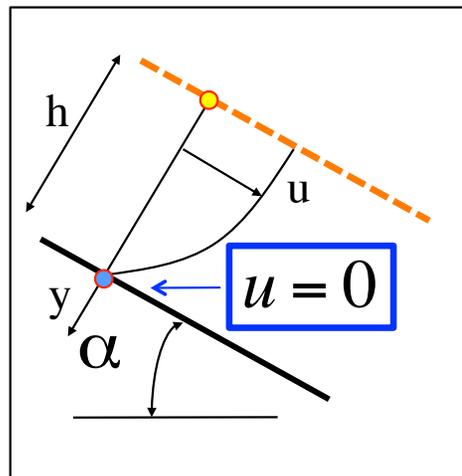
$$f_1(v; g_{12})$$

$T =$ “granular temperature”

$$f_4(v; g_{12})$$

$$N = \rho_s v g y \cos \alpha = f_4 \rho_s T$$

equation of state



$$u = \frac{2}{3} \left(\frac{\sqrt{v} f_4}{f_1} \tan \alpha \right) \frac{\sqrt{g \cos \alpha}}{d} (h^{3/2} - y^{3/2})$$

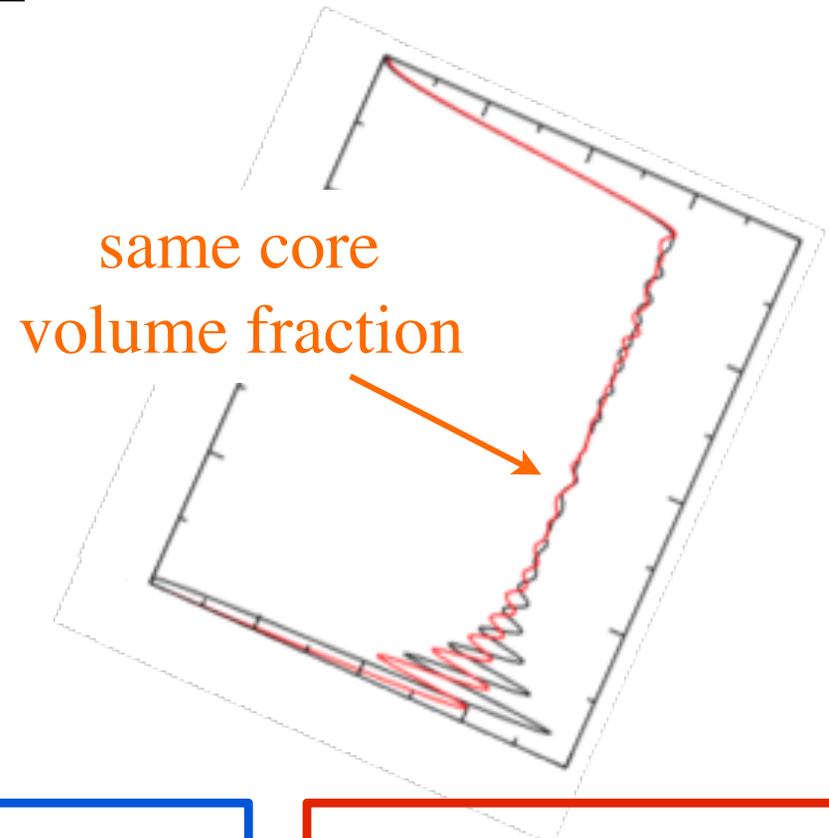
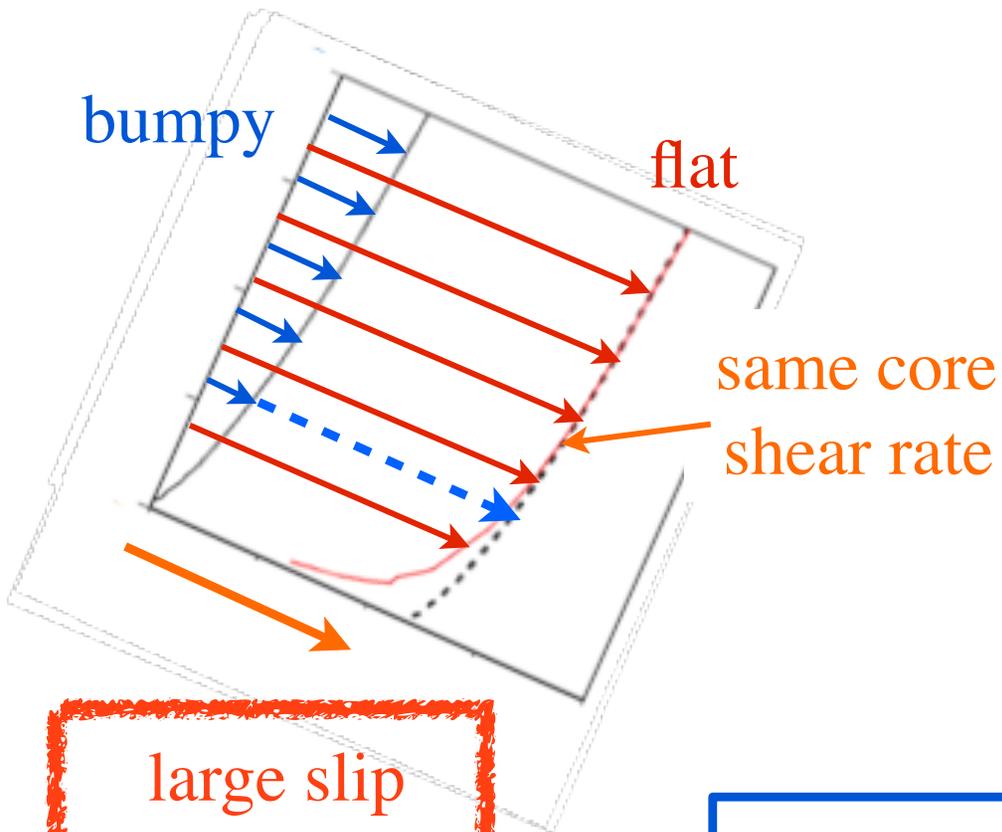
“Bagnold profile”

I

$$\frac{\dot{m}}{W} = \frac{2}{5} \frac{v^{3/2} f_4^{1/2}}{f_1} \frac{\rho_s g^{1/2}}{d} \frac{\sin \alpha}{\sqrt{\cos \alpha}} h^{5/2}$$

Flat, frictional base

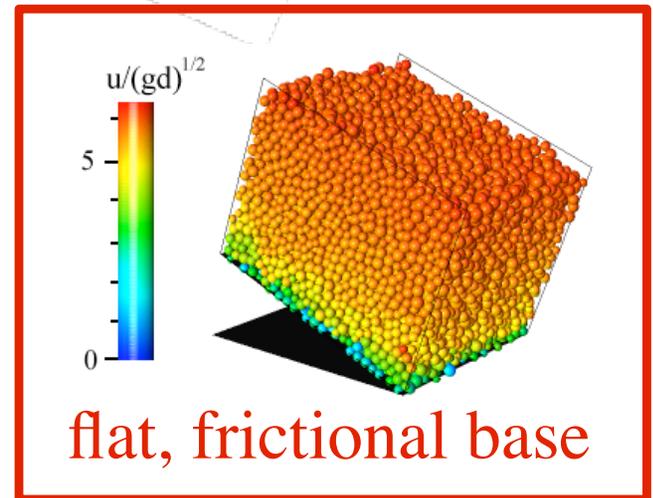
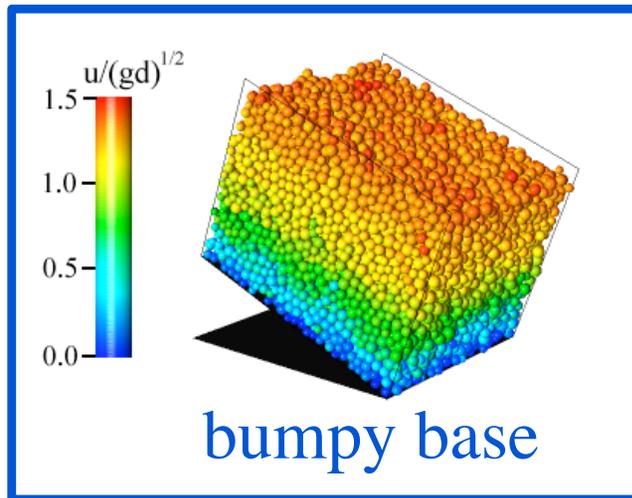
Delannay, et al, Nature Mat. 2007



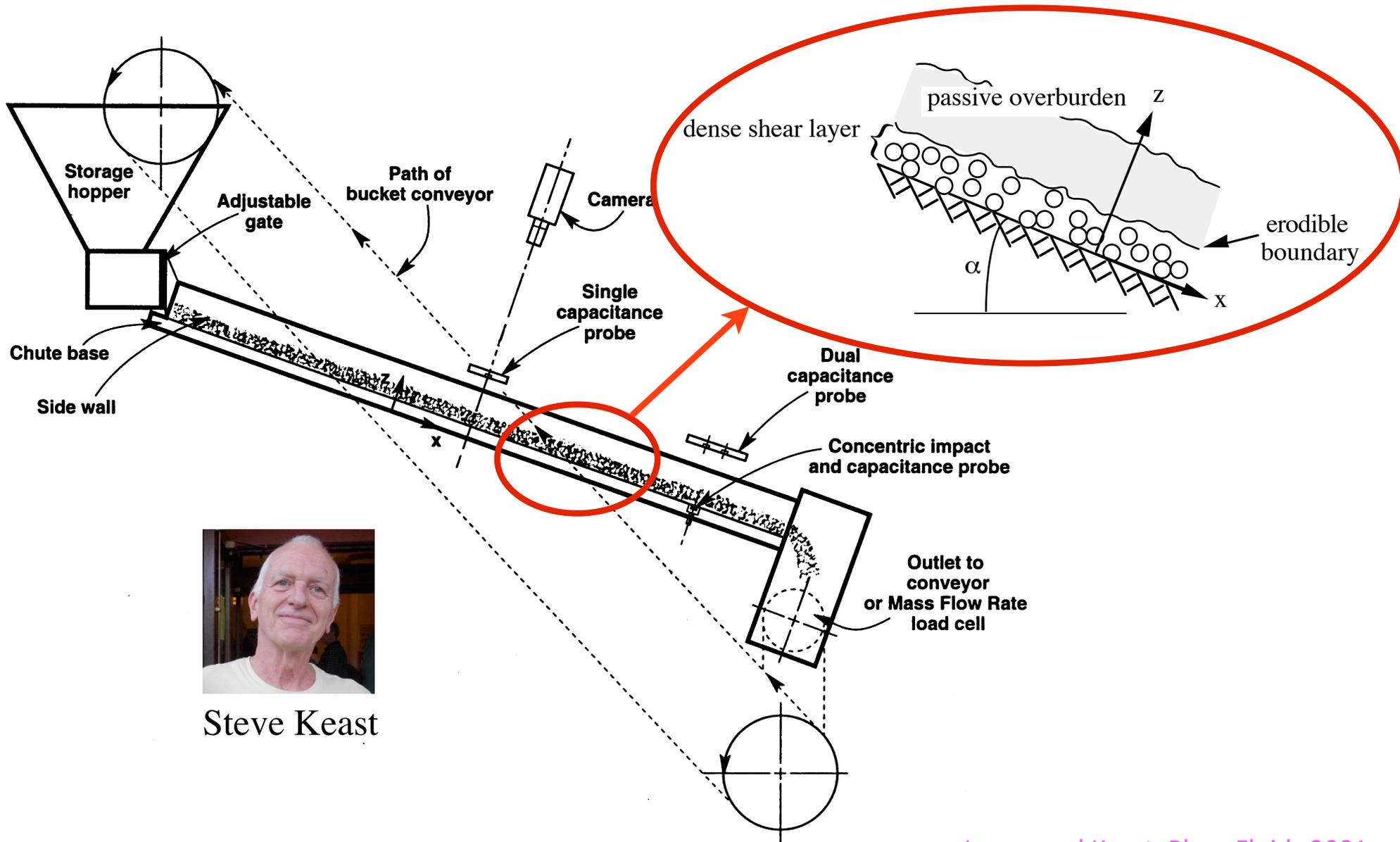
large slip at the bottom



Simulations:
Nicolas Taberlet



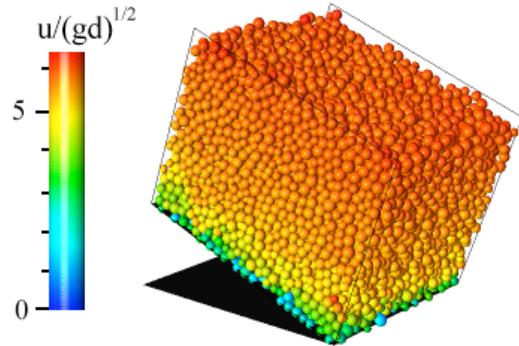
Flat, frictional base experiments



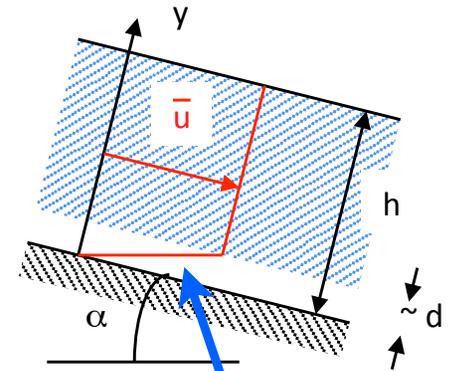
Steve Keast

Flat, frictional base cartoon

Louge and Keast, Phys. Fluids 2001



$$T_0 \sim \frac{\bar{v}}{f_4(v_0)} gh \cos \alpha$$



$$T_0, v_0$$

basal quantities

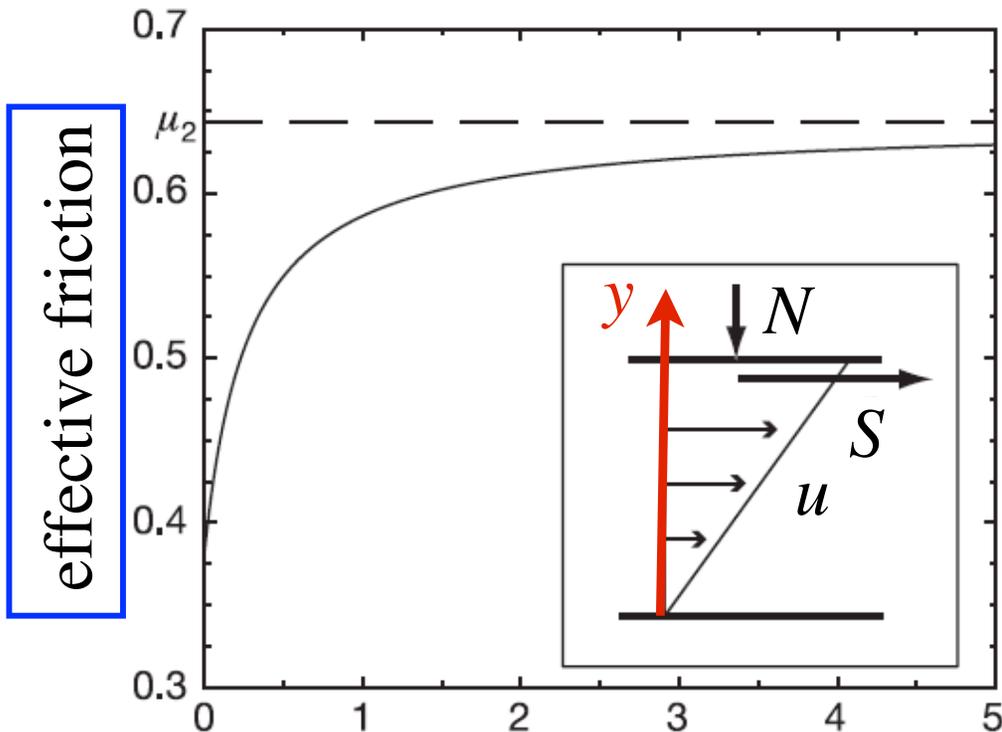
$$S \sim \rho_s gh \bar{v} \sin \alpha \sim f_1(v_0) \rho_s d \sqrt{T_0} \frac{\bar{u}}{d}$$

$$\text{Fr} = \frac{\bar{u}}{\sqrt{gh \cos \alpha}} \sim \left(\frac{\bar{v}^{1/2} f_4^{1/2}}{f_1} \right) \tan \alpha$$

length scale

$$\frac{\dot{m}}{W} \sim \rho_s g^{1/2} \frac{\bar{v}^{3/2} \sin \alpha}{\sqrt{\cos \alpha}} \left(\frac{f_4(v_0)^{1/2}}{f_1(v_0)} \right) h^{3/2}$$

Inertial number



$$I \equiv \frac{|du/dy| d}{\sqrt{N / \rho_s v}}$$

da Cruz, et al PRE 2005

Jop, Forterre & Pouliquen Nature 2006

GDR MiDi, Eur. Phys. J. E 2003

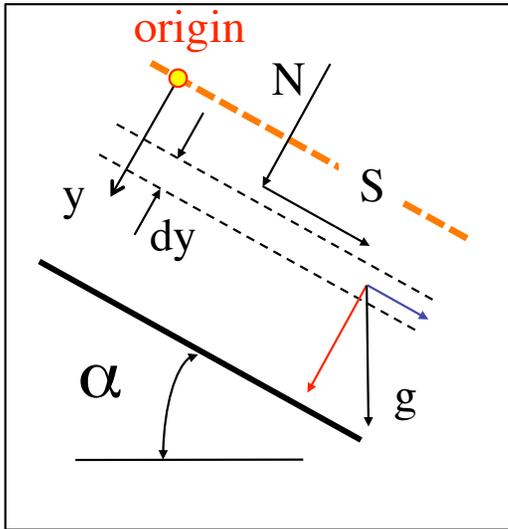
Chevoir, et al Powder Tech. 2009

Kamrin & Koval 2012

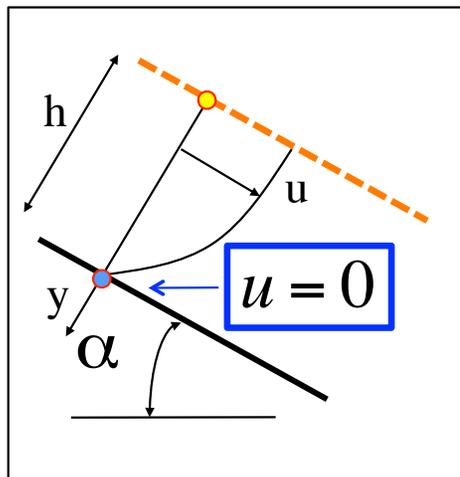
Bouzid et al 2013

Inertial number

Ralph Bagnold



bumpy base



$$u = \frac{2}{3} \left(\frac{\sqrt{\nu f_4}}{f_1} \tan \alpha \right) \frac{\sqrt{g \cos \alpha}}{d} \left(h^{3/2} - y^{3/2} \right)$$

I

“Bagnold profile”

“Non-local” extension

Kamrin & Koval 2012

Bouzid et al 2013

local fluidity

$$\mu = \frac{|du / dy|}{f}$$

“fluidity”

$$\nabla^2 f = \frac{f - f_0}{\xi^2}$$

length scale

Accounts for long-range interactions
and behavior at low shear rates.

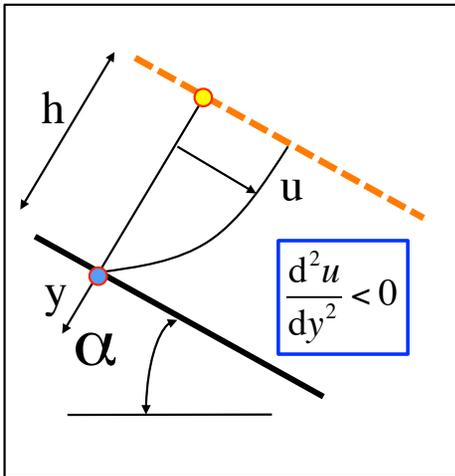
ξ and f_0 empirical functions

Boundary conditions?

Profile concavity and viscosity

$$S = \rho_s \nu g y \sin \alpha = -\mu \frac{du}{dy}$$

$$\frac{d^2 u}{dy^2} = -\rho_s g \sin \alpha \left(\frac{\nu y}{\mu} \right) \left[\frac{\nu'}{\nu} + \frac{1}{y} - \frac{\mu'}{\mu} \right]$$



bumpy base

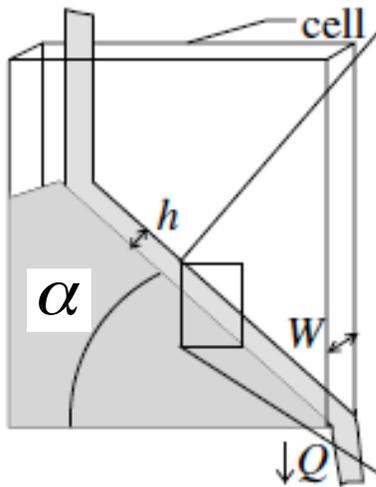
$$\frac{d^2 u}{dy^2} < 0 \Leftrightarrow \frac{d \ln \mu}{d \ln y} < \frac{d \ln \nu}{d \ln y} + 1$$

$$\frac{d \ln \mu}{d \ln y} = \frac{1}{2} \quad \frac{d \ln \nu}{d \ln y} = 0$$

Moderate increase in viscosity with depth for core flows over a bumpy base

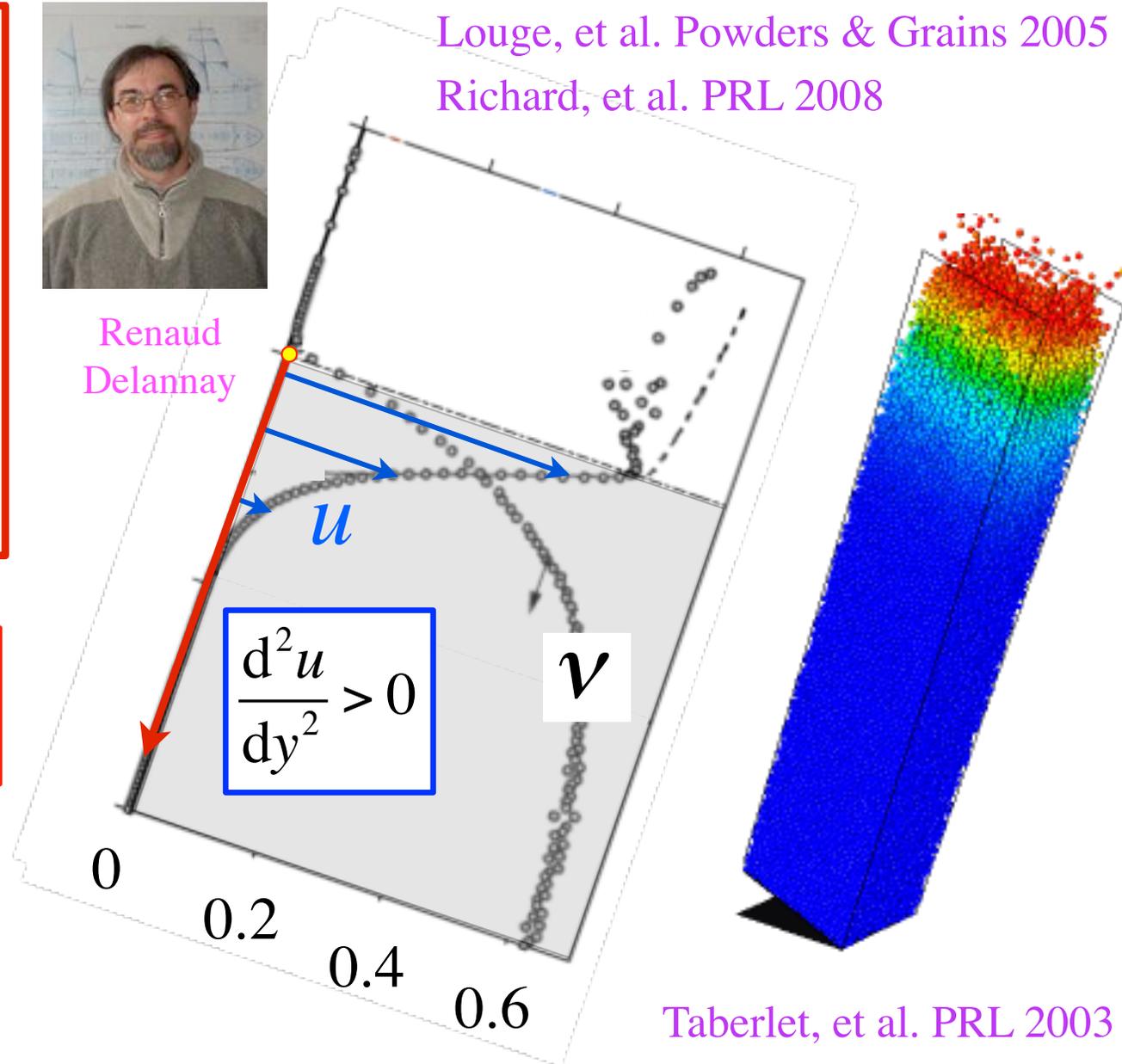
Inverted concavity for a soft base

Sidewall-stabilized heap



Renaud
Delannay

Louge, et al. Powders & Grains 2005
Richard, et al. PRL 2008



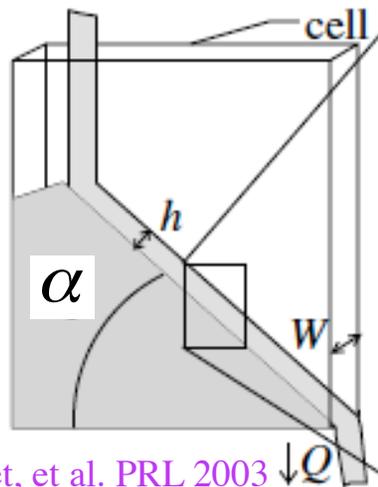
$$\frac{d^2u}{dy^2} > 0 \Leftrightarrow \frac{d \ln \mu}{d \ln y} > \frac{d \ln v}{d \ln y} + 1$$

Rapid increase in
volume fraction and
viscosity with depth.

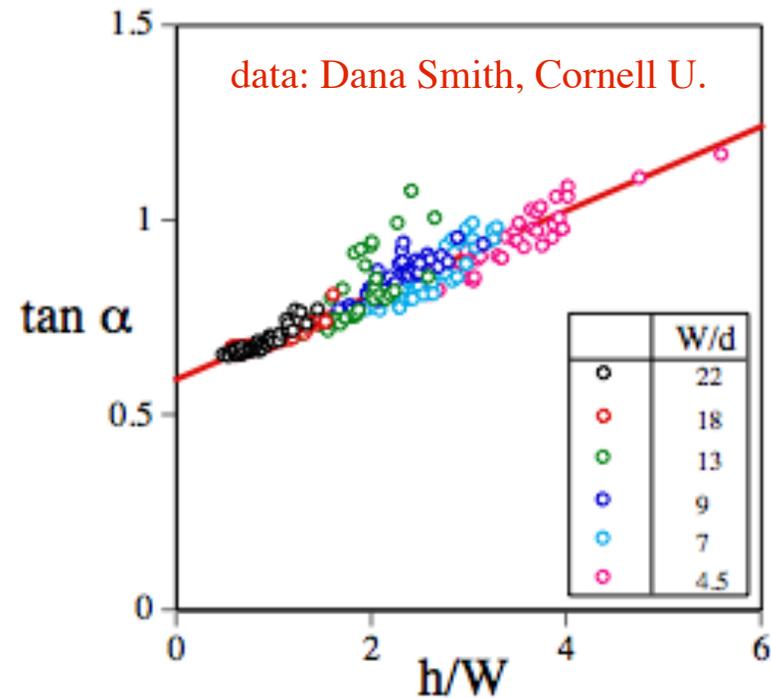
Taberlet, et al. PRL 2003

Role of side walls

Sidewall-stabilized heap



Taberlet, et al. PRL 2003



$$\tan \alpha = \mu_w \left(\frac{h}{W} \right) + \tan \alpha_{\min}$$

What about
an erodible base
with
far side walls?

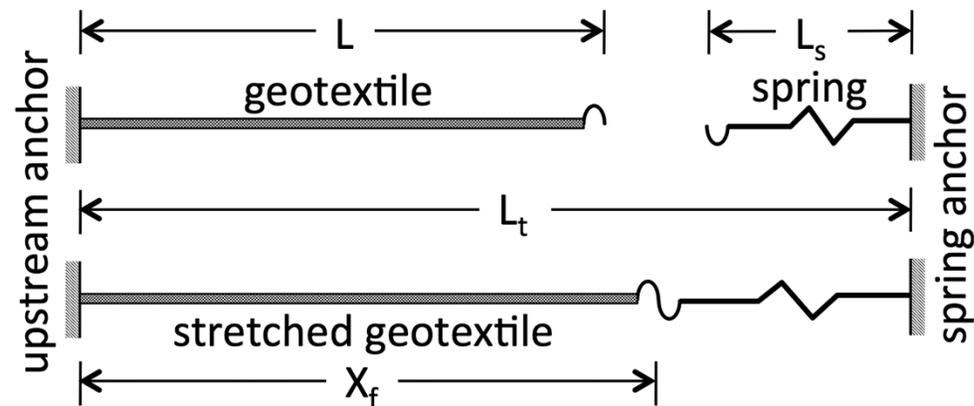
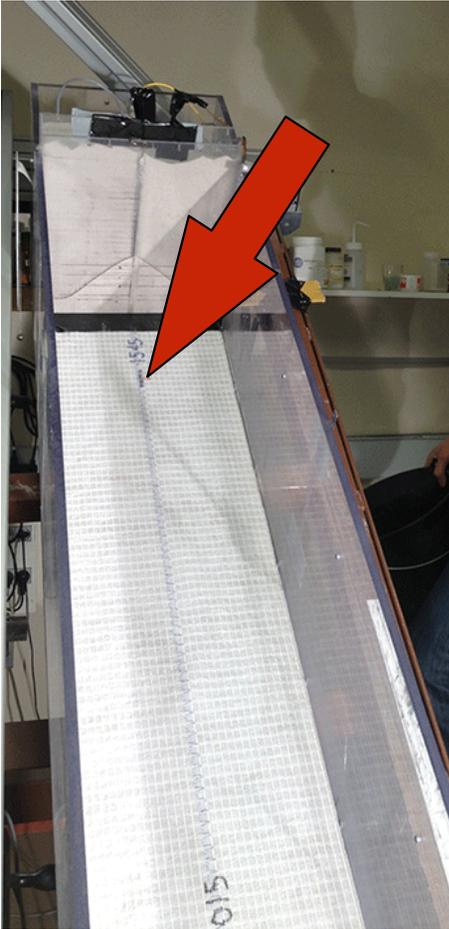




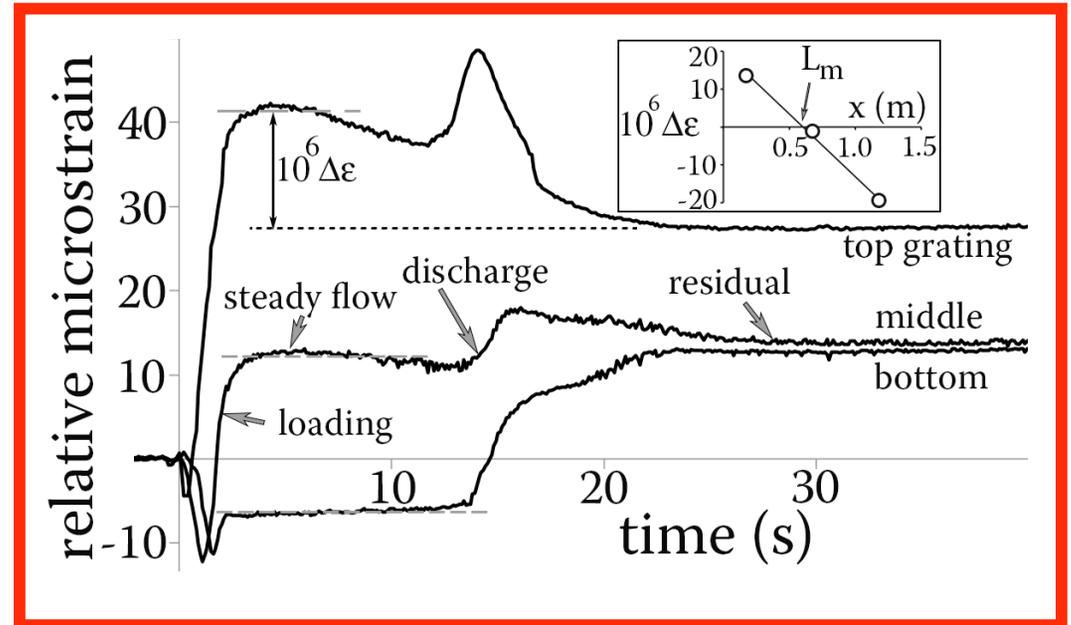
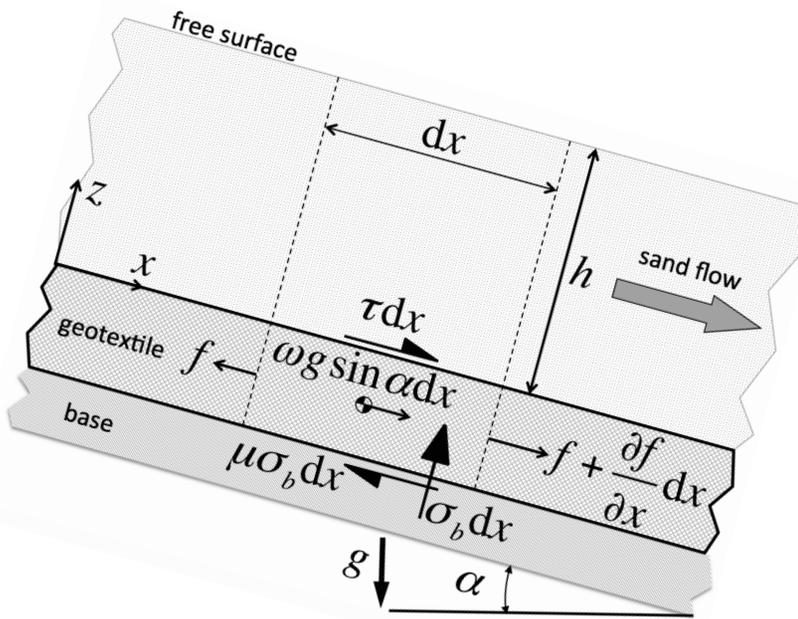
What about
an erodible base
with
far side walls?



Fiber-Bragg-grating geotextile



Fiber-Bragg-grating geotextile

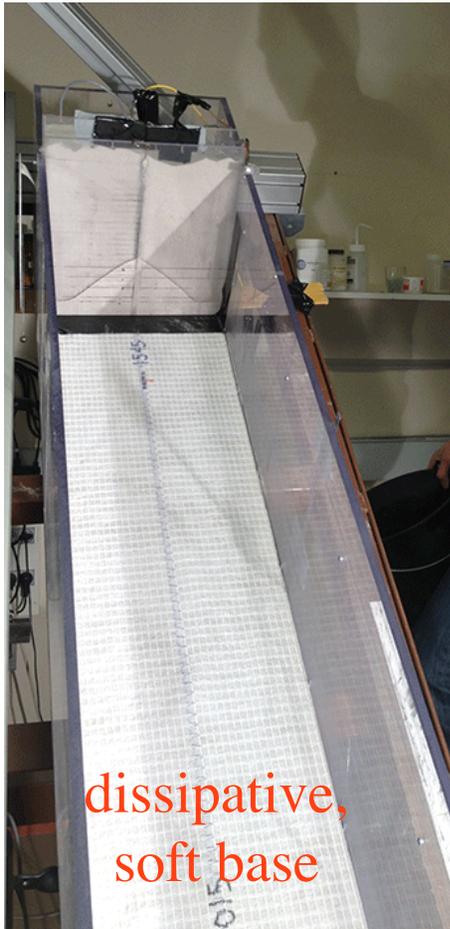


$$\Delta \varepsilon = \frac{(\tan \alpha - \mu)}{K} g \cos \alpha (H^\dagger - H_{\text{stop}}^\dagger) (L_m - x)$$

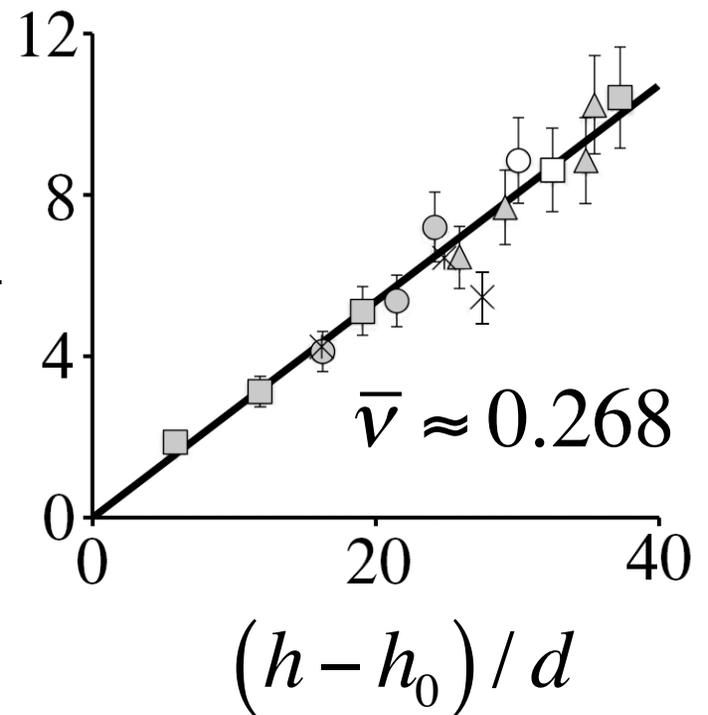
$$\Delta H^\dagger \equiv H^\dagger - H_{\text{stop}}^\dagger = \int_{h_0}^h v \frac{dy}{d}$$

Erodible base

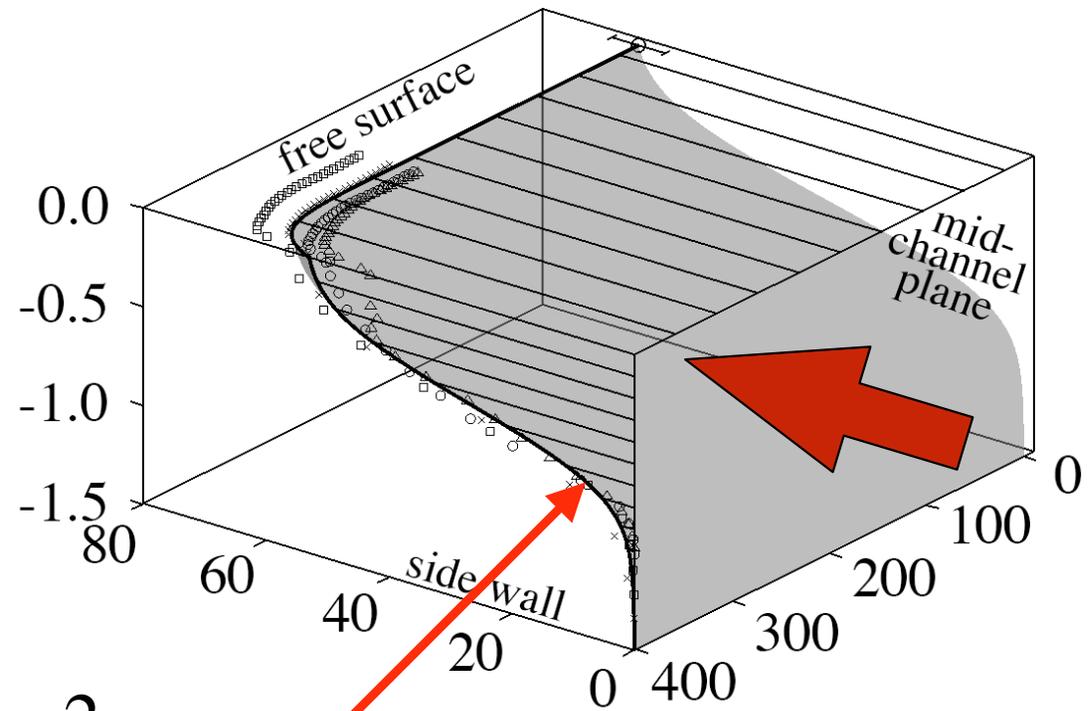
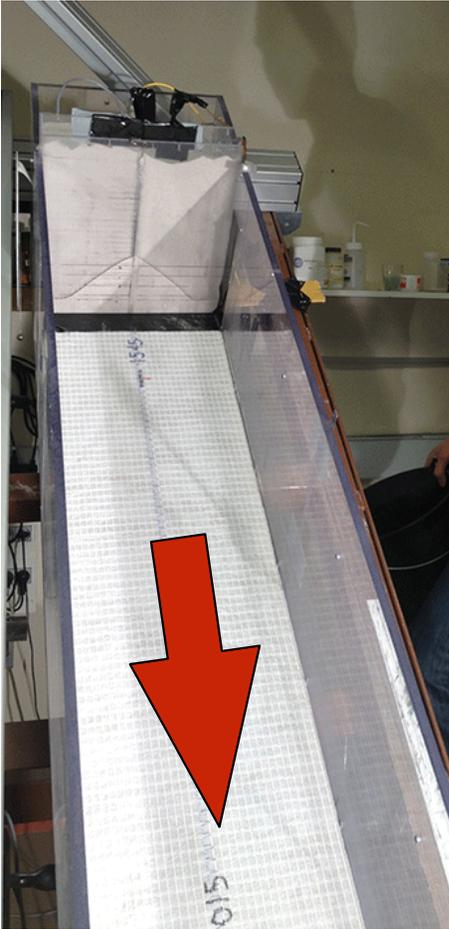
low mean volume fraction



$$\Delta H^\dagger = \int_{h_0}^h v \frac{dy}{d}$$



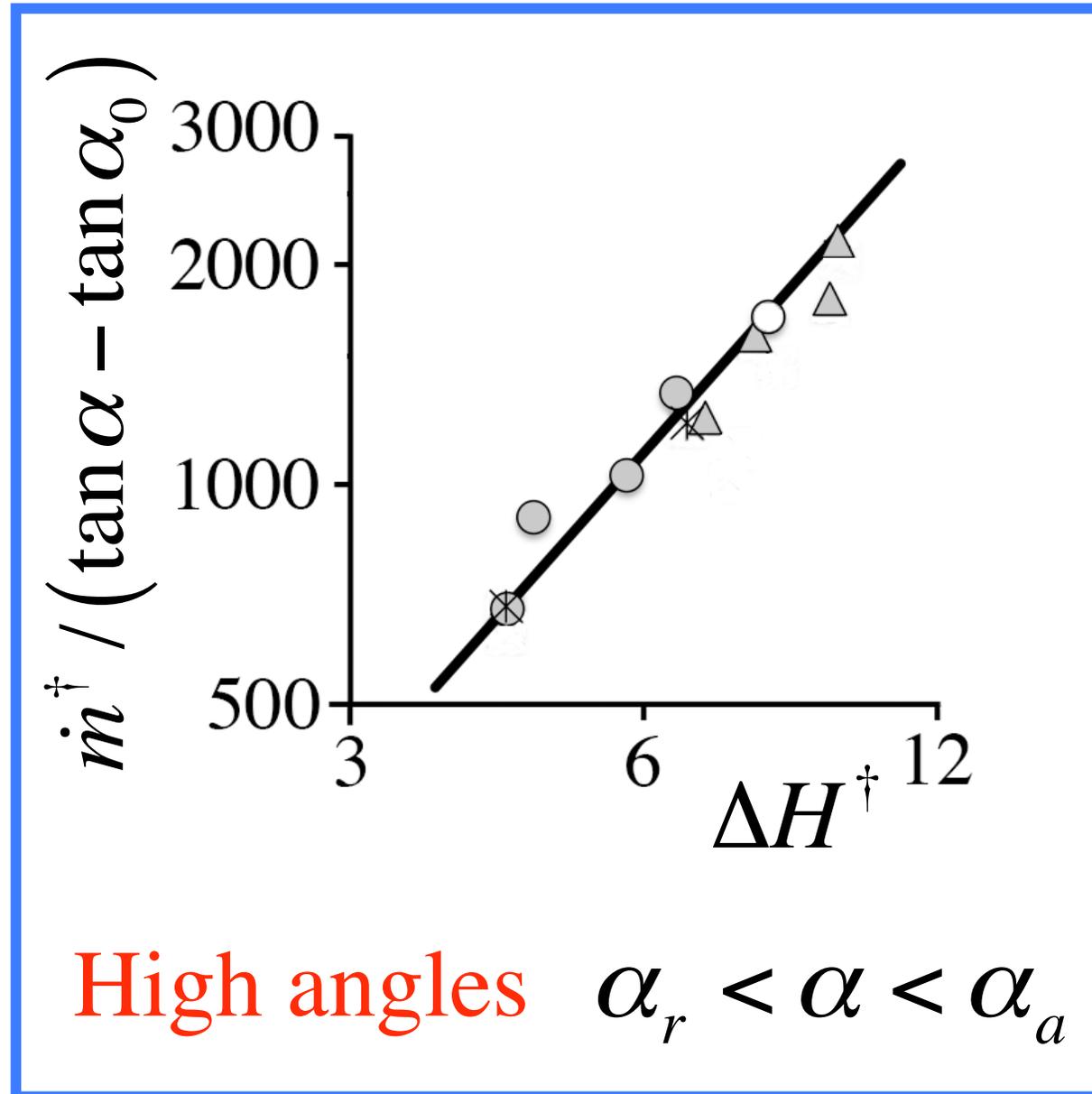
Erodible base



$$\frac{d^2 u}{dy^2} > 0$$

Erodible base

$$\dot{m} \propto \Delta H^{3/2} (\tan \alpha - \tan \alpha_0)$$

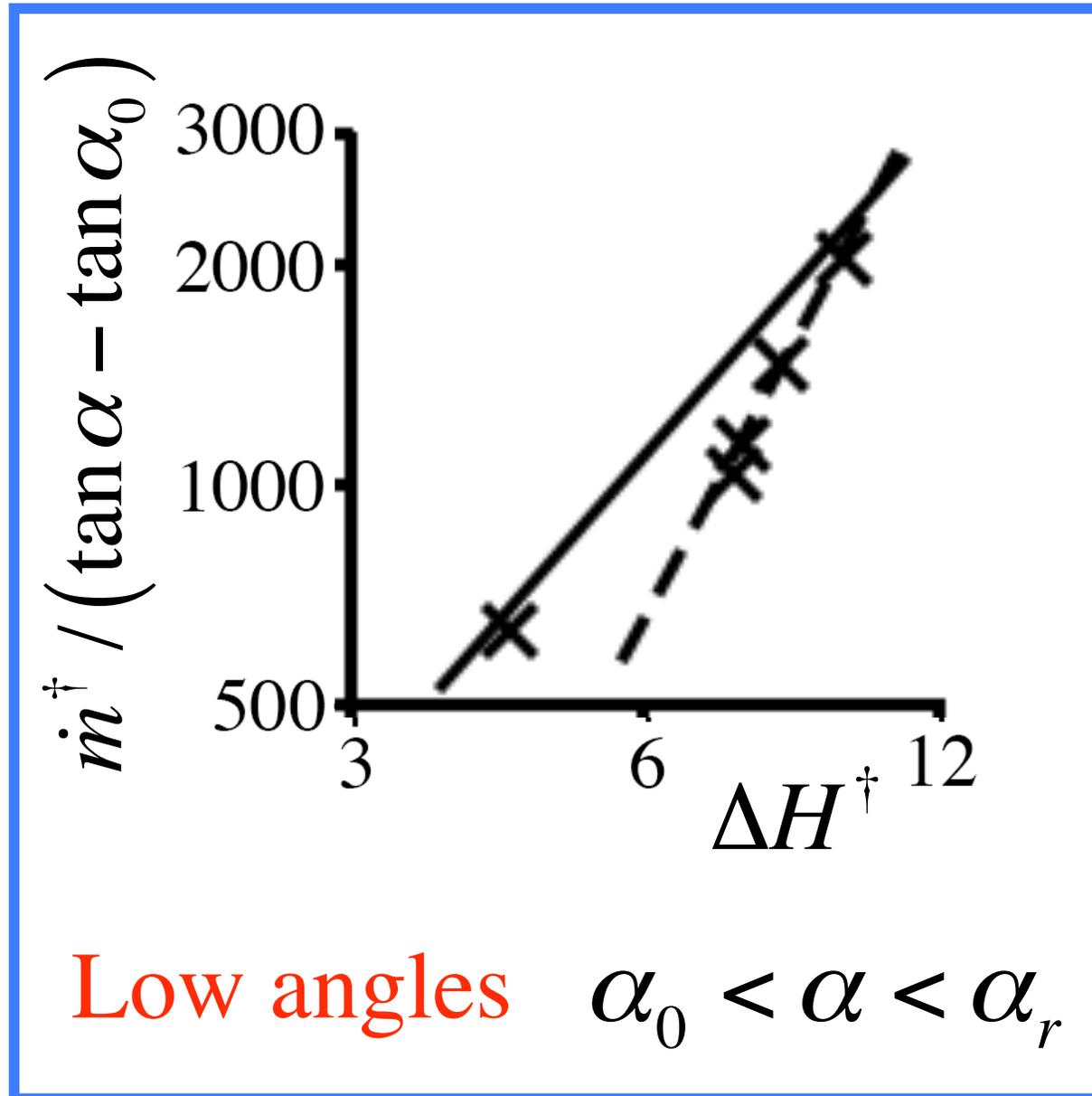


like
a flat wall

Erodible base

$$\dot{m} \propto \Delta H^{5/2} (\tan \alpha - \tan \alpha_0)$$

forced-fed
flows on
shallow
slopes



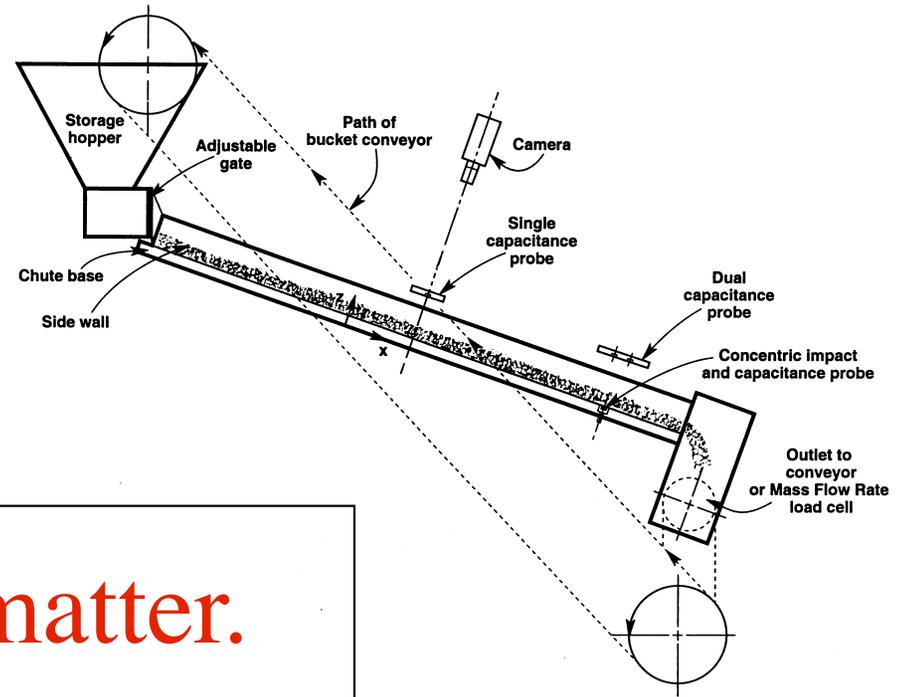
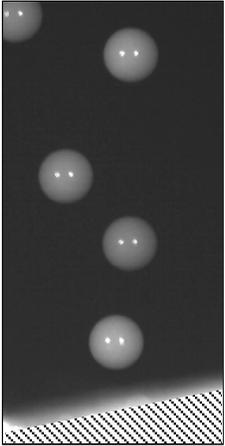
like a
bumpy
wall

Mass flow rate versus flowing depth

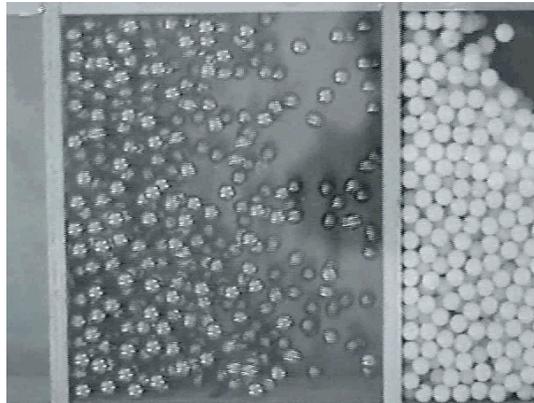
| flow type | n |
|-------------------------------------|-----|
| soft, dissipative base $> \alpha_r$ | 3/2 |
| Newtonian fluid, turbulent | 3/2 |
| flat, frictional base | 3/2 |
| soft, dissipative base $< \alpha_r$ | 5/2 |
| core over a bumpy base | 5/2 |
| Newtonian fluid, laminar | 3 |

$$\frac{\dot{m}}{W} \propto H^n$$

channel width W,
flowing depth H



Boundaries matter.



<http://grainflowresearch.mae.cornell.edu>